Bonding of Polyethylenimine in Covalent Organic Frameworks for CO₂ Capture from Air

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The COF exhibited a CO_2 capacity of 0.48 mmol g⁻¹ under dry conditions and 1.24 mmol g^{-1} under 75% relative humidity, both from simulated air containing 400 ppm of CO₂ at 25 °C. The CO₂ capacity and adsorption rate of COF-709 showed a strong relationship with the relative humidity in the



environment, in accordance with the CO_2 adsorption mechanism revealed by ssNMR. The chemical stability of C-S bonds utilized to covalently install the polyamine in COF pores prevented its amine loss and hydrolysis, giving COF-709 an excellent cycling stability, which was confirmed by applying 10 adsorption-desorption cycles under simulated direct air capture conditions, showing no uptake loss.

INTRODUCTION

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Atmospheric carbon dioxide concentrations have increased by more than 50% since the 18th century, resulting in substantial environmental issues.^{1,2} Direct air capture (DAC) of CO₂ is one of the most targeted and effective methods to tackle this problem.³⁻⁵ Among all CO₂ adsorption candidates, polyethylenimine (PEI) is one of the most competitive materials due to its high adsorption capacity, low regeneration temperature, and low material cost.⁶⁻⁸ Current techniques utilize aqueous PEI solutions for CO₂ capture, but their practical application is hindered by low mass-transfer rates caused by increased viscosity during CO₂ adsorption and amine corrosion.9,10 Extensive research has therefore focused on using PEI-functionalized solid-state materials, such as zeolites, 11,12 silica, $^{13-15}$ alumina, 16,17 and metal–organic frameworks (MOFs), 18,19 for DAC of CO₂. Two approaches, amine impregnation and amine grafting, have been developed to load PEI onto solid supports.^{20,21} In PEI-impregnated sorbents, PEI is attached to the solid supports through weak van der Waals and hydrogen bonding interactions, which results in amine loss in the presence of water.²² In PEI-grafted sorbents, however, the amine loading density is limited due to the incomplete coupling reaction between PEI and the solid support, leading to a low CO2 capacity under DAC conditions.²³ Additionally, the hydrophilic nature of current

polyamine-functionalized sorbents causes degradation of their surface and pore structures at high relative humidity, resulting in decreased performance during cycling.²⁴ Thus, it is essential to develop a reliable strategy for covalently binding PEI within the pores of sorbents to prevent amine loss and potential hydrolysis of the bonds between the amines and the sorbentaspects that have plagued the current amine-functionalized systems.

Here, we designed and synthesized a PEI-functionalized covalent organic framework (COF), termed COF-709. By conducting aromatic nucleophilic substitution (S_NAr) on the COF pore walls, thiol-modified branched polyethylenimine (SH-bPEI) was successfully installed inside the pores of COF-709 through chemically stable C-S covalent bonds. The resulting COF captures 1.24 mmol g⁻¹ CO₂ from simulated air containing 400 ppm of CO_2 with 75% relative humidity (RH) at 25 °C. The strong covalent bonding between the polyamine and the framework, along with the hydrophobic nature of the

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Figure 1. (a) Synthetic scheme and (b) structure of COF-709; (c) stacked FT-IR spectra of imine-COF-709, amide-COF-709, and COF-709; and (d) ¹⁹F spin echo solid-state NMR of imine-COF-709, amide-COF-709, and COF-709. a.u., arbitrary units.

sorbent, contributes to the excellent cycling stability of COF-709. This was confirmed by performing 10 CO₂ adsorption–desorption temperature-swing cycles (25–95 °C) in simulated air, with full retention of its CO₂ capacity.

In this context, COFs are excellent candidates for CO_2 capture, as their pore structures and environments can be precisely tuned through reticular design.²⁵ Others and we have shown that multiple amine-functionalized COFs have been synthesized, showing improved CO_2 capture performance after amine loading.^{26–29} However, their CO_2 capacity under DAC conditions (CO_2 concentration around 400 ppm) remains low, mainly due to the low amine loading density and a lack of strong chemisorption sites in the material. A recent contribution from our group involved the in situ polymerization of polyamine in COFs, demonstrating how chemically stable covalent bonds between the PEI and COF provide for a robust performance.³⁰ The approach we report in this

contribution adds yet another strategy to addressing the shortcomings of the materials highlighted above by using the chemically stable C-S bonds in the covalent attachment of PEI to the COF's pores.

RESULTS AND DISCUSSION

Design and Synthesis. COF-709 was synthesized by the crystallization of an imine-linked COF backbone, followed by postsynthetic linkage oxidation and polyamine installation (Figure 1a, see details in Section S2, Figures S23–S25). First, a porous, crystalline imine-linked COF precursor, imine-COF-709, was crystallized through imine condensation between 2',3',5',6'-tetrafluoro-[1,1':4',1''-terphenyl]-4,4''-dicarbalde-hyde (TFTDA) and 1,3,6,8-tetrakis(4-aminophenyl)pyrene (TAPPy). The crystallization was conducted in 1,4-dioxane and catalyzed by acetic acid for 3 days. In the second step, imine-COF-709 was oxidized by reacting with an aqueous



Figure 2. (a) PXRD patterns, (b) N_2 sorption isotherms (77 K), and (c) single-component CO₂ isotherms (25 °C) of imine-COF-709, amide-COF-709, and COF-709 and (d) single-component H_2O isotherm of COF-709 at 25 °C. The inset in panel (c) displays a zoomed-in view of the CO₂ sorption isotherm of COF-709 highlighting the uptake at the ambient CO₂ pressure (0.4 mbar). a.u., arbitrary units; P/P_0 , relative nitrogen pressure; $P_0 = 1$ atm; STP, standard temperature and pressure; and P/P_{satr} relative water vapor pressure.

sodium chlorite solution to afford amide-COF-709.³¹ The complete conversion from imine linkage to amide linkage enhanced the chemical stability of the COF backbone during the subsequent polyamine loading process and DAC applications. Finally, SH-bPEI was covalently installed on the COF backbone with C–S bonds through an aromatic nucleophilic substitution, catalyzed by sodium hydride, to obtain COF-709 (Figure 1b).

Fourier transform infrared (FT-IR) spectroscopy was first utilized to investigate the completeness of the reactions at each stage (Figures 1c and S1). The FT-IR spectrum of imine-COF-709 showed an emergence of imine $\nu_{C=N}$ stretch at 1625 cm⁻¹ and a notable decrease in the intensity of vibrational absorbance bands at 1700 cm⁻¹ (aldehyde $\nu_{C=O}$ stretch) observed in TFTDA, as well as the broad absorbance bands at 3500–3200 cm⁻¹ (amine ν_{N-H} stretch) in TAPPy (Figure S1). These observations signified the conversion of aldehyde and amine moieties in the starting materials, confirming the formation of imine linkages in imine-COF-709. After the linkage oxidation step, the vibrational absorbance bands at 1625 cm⁻¹ in amide-COF-709 largely diminished, corresponding with the observation of an emerging carbonyl $\nu_{C=O}$ stretch at 1657 cm⁻¹, validating the conversion of imine to amide linkages (Figure 1c). In the last step, the FT-IR spectrum of COF-709 showed higher-intensity absorbance bands at 2928 and 2820 cm⁻¹, which are assigned to the alkane ν_{C-H} stretch, indicating the introduction of aliphatic SH-bPEI in COF-709. The formation of C–S bonds between SH-bPEI and COF backbone was confirmed by the decreased intensity of absorbance bands at 980–975 cm⁻¹ (ν_{C-F} stretch) in COF-709, ³² corroborating the covalent bonding between SH-bPEI and COF-709.

The two-step postsynthetic linkage oxidation and polyamine installation were further characterized by solid-state nuclear magnetic resonance (ssNMR) spectroscopy. The complete oxidation from imine to amide linkages was confirmed by the disappearance of the imine peak at 158 ppm of ¹³C labeled imine-COF-709 and the emergence of a characteristic amide peak observed at 164 ppm of ¹³C labeled amide-COF-709 in the ¹³C ssNMR spectra (Figure S17). The aromatic nucleophilic substitution polyamine installation reaction was monitored with both ¹³C and ¹⁹F ssNMR spectra. The newly emerged signals between 67 and 29 ppm in the ¹³C ssNMR spectrum of COF-709, which were assigned to the aliphatic C atoms in SH-bPEI, signified the successful incorporation of polyamine in COF-709 (Figure S18).³³ The covalent



Figure 3. (a) CO₂ dynamic breakthrough curves and (b) calculated CO₂ uptake under 400 ppm of CO₂ with 0, 10, 25, 50, and 75% RH at 25 °C for COF-709. (c) CO₂ uptake under humid simulated air (400 ppm of CO₂ with 75% RH) at 25 °C derived from 10 temperature-swing cycling breakthrough measurements, giving an average working capacity of 1.23 mmol g^{-1} (dotted line).

installation of SH-bPEI was evidenced by the shifted signal at 106 ppm in ¹⁹F ssNMR of COF-709 (Figure 1d), which was assigned to the remaining F atoms on the sulfur-substituted benzene rings in COF-709, confirming the formation of C–S bonds between SH-bPEI and the COF.³⁴ The amount of active amine sorption sites installed on COF-709 was quantified to be 9.24 mmol per gram of sorbent through elemental analysis (see Section S9 for details), and the chemical formula of COF-709 can be written as $C_{40}H_{21}N_2O_2F_{1.21}(SCH_2CH_2)_{2.79}(C_2H_5N)_{9.24}$.

The structures of the COF-709 series were characterized through a combination of analyses, including powder X-ray diffraction (PXRD), N₂ sorption isotherms, scanning electron microscopy (SEM), and thermogravimetric analysis (TGA). The crystallinity of imine-COF-709 was evaluated by a PXRD analysis (Figure 2a). The framework was modeled in the C2/mspace group,³⁵ and Pawley refinement was applied to the experimental pattern, providing the unit cell parameters of a =48.416(1) Å, b = 44.411(5) Å, c = 3.80(3) Å, $\alpha = \gamma = 90^{\circ}$, and $\beta = 81.7^{\circ}$ with $R_{p} = 7.91\%$ and $R_{wp} = 10.96\%$ (Figure S3 and Table S1). The PXRD peaks at 2.5°, 3.5°, 5.2°, 7.8°, 10.6°, 13.3°, and 23.3° were assigned to the (110), (200) and (020), (220), (330), (440), (550), and (001) lattice planes, respectively. These observations are consistent with the simulated structure, in which TFTDA and TAPPy are connected by imine linkages, forming square lattice sheets that stack in the AA stacking mode. SEM images revealed that imine-COF-709 forms uniformly aggregated particles, suggesting a homogeneous composition (Figure S2). COF-709 series showed no significant weight loss below 300 °C, confirming their high thermal stability (Figure S16).

The N₂ sorption isotherm measurements on imine-COF-709 at 77 K revealed a Brunauer–Emmett–Teller (BET) surface area of 1880 m² g⁻¹, with a pore size of 3.0 nm, which is in good agreement with the modeled pore size of the AA stacking mode (Figures 2b and S5). The crystallinity of amide-COF-709 was largely retained, with a BET surface area of 1157 m² g⁻¹ (Figure S6). The lowered BET surface area can be attributed to the increase in framework mass and reduced pore volume.³⁰ Notably, the PXRD pattern of amide-COF-709 remained unaltered after immersion in various basic solutions, demonstrating its chemical robustness (Figure S22). After SHbPEI installation, the framework composition was unaffected (Figure S18), and the PXRD pattern of COF-709 showed noncrystalline features, and its N₂ isotherm showed limited porosity (Figure S7), which can be explained by the high flexibility of the large number of polyamines introduced to its pore channels. Despite its limited accessibility to N_2 , the robustness of the COF backbone and the large amount of polyamine covalently installed in the pore channels made the resulting sorbent, COF-709, promising for the DAC application of CO₂.

CO₂ and Water Isotherm Measurements. The CO₂ capture capability of our sorbent, COF-709, was initially evaluated through a single-component CO₂ gas sorption isotherm measurement at 25 °C (Figure 2c). The CO₂ isotherm of COF-709 showed a steep increase in the adsorption curve at CO₂ pressures below 1 mbar, reaching an inflection point between 1 and 10 mbar, followed by a moderate increase at higher CO2 pressures between 10 and 1000 mbar. Hysteresis between the adsorption and desorption curves was observed at all CO₂ pressures. These observations suggest strong chemical interactions between COF-709 and CO_2 . Based on the single-component adsorption data, the CO_2 capacity of COF-709 is 0.44 mmol g^{-1} at 0.4 mbar (400 ppm, concentration close to the CO₂ pressure in atmospheric conditions) and 1.77 mmol g^{-1} at 40 mbar (4%, concentration close to natural gas flue). The isosteric heat of CO₂ adsorption is calculated to be 41-50 kJ mol⁻¹ (Figure S10) according to the CO₂ adsorption isotherms of COF-709 at 15, 25, and 35 °C (Figure S9). At 25 °C, the water uptake of COF-709 was 0.07 $g_{water} g_{COF}^{-1}$ at 50% RH and 0.13 $g_{water} g_{COF}^{-1}$ at 75% RH (Figure 2d). The low water uptake allows for low energy input in the regeneration step upon cycling.³⁶ The water isotherm of COF-709 was also measured at various temperatures (Figure S11), and the isosteric heat of water vapor adsorption is calculated to be 48 kJ mol⁻¹ (Figure S12).

Dynamic Breakthrough Measurements. To further evaluate the CO_2 capture performance of COF-709 for practical DAC applications, multicomponent dynamic breakthrough measurements were conducted, simulating practical DAC conditions where humidified gas flow continuously passes through the sorbents. First, CO_2 and water vapor dynamic breakthrough curves were measured under simulated atmospheric conditions, with 400 ppm of CO_2 balanced in synthetic air ($N_2/O_2 = 4/1$) under different RH at 25 °C (Figure S13). After being exposed to the gas flow, COF-709 adsorbed both CO_2 and water vapor. The material rapidly attained its maximum capacity for water vapor, while CO_2 remained trapped in the pores until breaking through, marked by a sharp increase in outlet CO_2 concentration. The outlet $\rm CO_2$ concentration eventually reached 395 ppm, marking the point at which the saturated adsorption capacity for $\rm CO_2$ was achieved. The amount of $\rm CO_2$ captured during the break-through measurements was calculated through numerical integration of the difference between the inlet and outlet $\rm CO_2$ concentrations.

The influence of water content in the simulated air on CO_2 adsorption was assessed by measuring the CO₂ breakthrough behavior of the same batch of COF-709 across different RH, ranging from 0 to 75% at 25 °C (Figure 3a,b). The inlet CO₂ concentration was controlled at 400 (± 2) ppm for all experiments. Under dry conditions (0% RH), COF-709 showed a CO_2 uptake of 0.48 mmol g⁻¹, which is 9% higher than its single-component CO_2 uptake of 0.44 mmol g⁻¹. This can be attributed to the pressure increase when feed gas was passed through the packed column, as the column pressure reached 1.15 atm during the breakthrough analysis (Figure S13). When water vapor was introduced in the feed gas, the CO₂ capacity of COF-709 increased significantly with the increase of RH level, reaching 1.24 mmol g⁻¹ at 75% RH, marking a 2.58-fold increase compared with its dry uptake. This CO₂ uptake increase under humid conditions is higher than those of other reported DAC sorbents so far, to the best of our knowledge. In addition to the CO₂ capacity, the different shapes of the breakthrough curves under various RH levels also indicate varying adsorption kinetics. At higher RH, the rate at which the outlet CO₂ concentration increases after breakthrough is significantly accelerated. These observations clearly demonstrate that the water content in the simulated air is strongly and positively correlated to the CO₂ capacity and adsorption kinetics of COF-709.

Given the high CO₂ uptake and fast adsorption kinetics of COF-709 at high RH levels, the cycling stability test of COF-709 was performed by applying 10 consecutive adsorptiondesorption temperature-swing cycles in simulated air (400 ppm of CO₂ at 75% RH and 25 °C) (Figures S14 and S15). For each cycle, after reaching its saturated CO₂ capacity, the COF sorbent was regenerated at a column wall temperature of 95 °C and a sorbent inner temperature of 60 °C under continuous N2 flow. The adsorption and regeneration steps were set to end when the outlet CO_2 concentration reached 395 and 5 ppm, respectively. The CO₂ capacity of COF-709 was determined to be 1.23 mmol g^{-1} cycle⁻¹ over 10 consecutive cycles with no uptake loss, confirming its high stability under DAC conditions (Figure 3c and S15). This result also demonstrated that a low regeneration temperature of 95 °C is sufficient to regenerate COF-709, due to its hydrophobic nature, allowing for low energy input in the removal of water molecules.

Adsorption Mechanism Study. To understand the reasons for the higher adsorption capacity of COF-709 under humid conditions, ¹³C ssNMR spectroscopy was employed to study the adsorption species of CO₂ in COF-709 under both dry and humid conditions (Figure S19). Specifically, COF-709 was first fully activated at 100 °C under vacuum to remove adsorbed CO₂, before being exposed to dry ¹³CO₂ at 25 °C for 3 h. For humid conditions, COF-709 samples were first presaturated with water at 80% RH in N₂, followed by exposure to ¹³CO₂. Under dry conditions, two signals at 163.7 and 159.8 ppm were observed in the ¹³C spectrum, which can be attributed to the formation of carbamate and carbamic acid as a result of the reaction between CO₂ and the SH-bPEI in COF-709 (Figure S20).³⁷ In contrast, under humid conditions, COF-709 exhibited two intensive signals at 165.0 and 164.2

ppm, indicating the formation of bicarbonate and carbamate, respectively (Figure S21).³⁸ These results are in agreement with previous mechanism studies on the reaction between CO_2 and polyamine,^{39,40} where under dry conditions, the major products of the reaction between CO_2 and COF-709 are carbonate/carbamic acid pairs, whereas the introduction of water converts the pairs into bicarbonate, shifting the adsorption equilibrium and thereby increasing the CO_2 adsorption capacity.

CONCLUSIONS

We employed a new postsynthetic polyamine installation strategy in COF-709 by performing aromatic nucleophilic substitution within the COF pore channels. This strategy employing C–S bonds between the framework and the amine entity overcomes the challenges associated with amine loss and hydrolysis. The resulting sorbent, COF-709, exhibited exceptional CO₂ capacity when exposed to ambient air under both dry and humid conditions. The CO₂ capacity of COF-709 is strongly and positively correlated with RH in the air. The sorbent also demonstrated excellent cycling stability and low regeneration temperature under simulated DAC conditions. This research not only provided a promising CO₂ sorbent for DAC application but also revealed significant potential of amine functionalization in advancing the development of porous sorbents for DAC applications.

ASSOCIATED CONTENT

Data Availability Statement

The raw data for the ¹⁹F solid-state NMR experiments are available on Zenodo (https://doi.org/10.5281/zenodo. 14112789).

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/jacs.4c14971.

Detailed experimental procedures, synthesis, and characterization details of the reported compounds, including FT-IR, SEM, PXRD analysis and refinement, solution-state NMR, TGA, calculation of amine loading density, solid-state NMR, nitrogen sorption isotherms, water vapor sorption isotherms, CO_2 sorption isotherms, and dynamic breakthrough measurements (PDF)

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Author Contributions

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Notes

The authors declare the following competing financial interest(s): O.M.Y. is co-founder of ATOCO Inc., aiming at commercializing related technologies.

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